

A better whey:

The production of multiple high-value products from Greek yogurt acid whey *via* filtration and acid-catalyzed lactose hydrolysis

Mark Lindsay

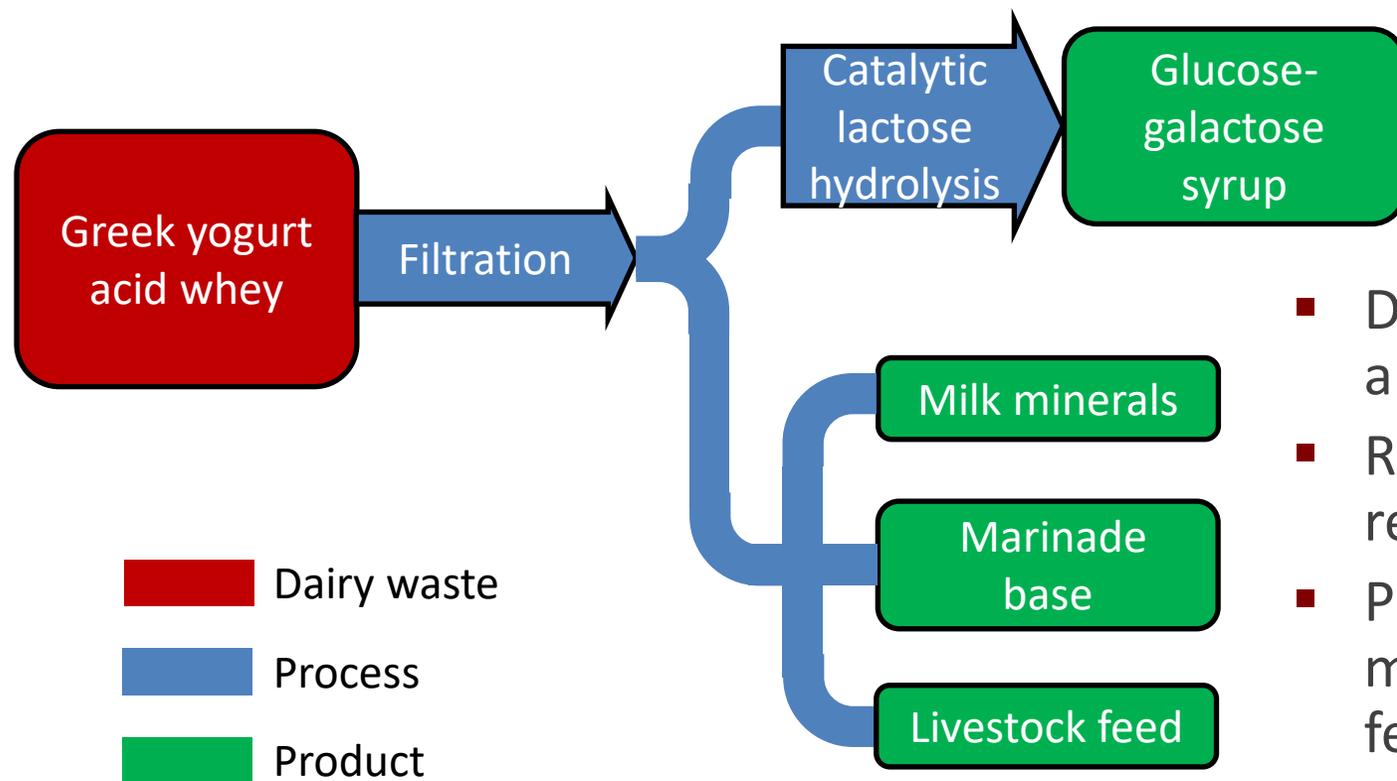
Product Development Technologist at Wells Enterprises, Inc

PhD of Chemical Engineering from UW-Madison

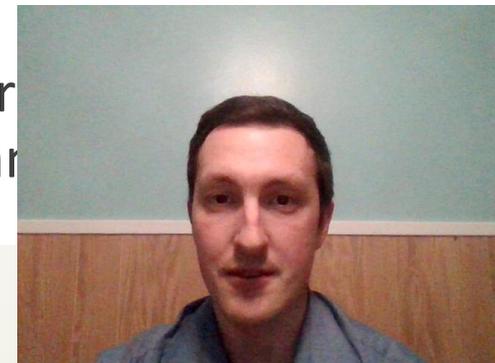
(Dr. George Huber and Dr. Scott Rankin, advisors)

October 26, 2021





- Demonstrated technology in pilot plant and laboratory continuous flow reactor
- Rigorous economic model shows potential revenues of \$19 million/year
- Products are glucose-galactose syrup, milk minerals, a marinade base, and a livestock feed
- **Validated glucose-galactose syrup for use in soft-serve ice cream**
- Looking for partners interested in commercializing the technology





George Huber

- Professor of Chemical and Biological Engineering
- Catalysis expert



Scott Rankin

- Professor of Food Science
- Department chair of Food Science Department
- Expert in Dairy Science



Jarryd Featherman

- Recent UW-Madison Chemical Engineering graduate
- Heads process scale-up and industrial outreach

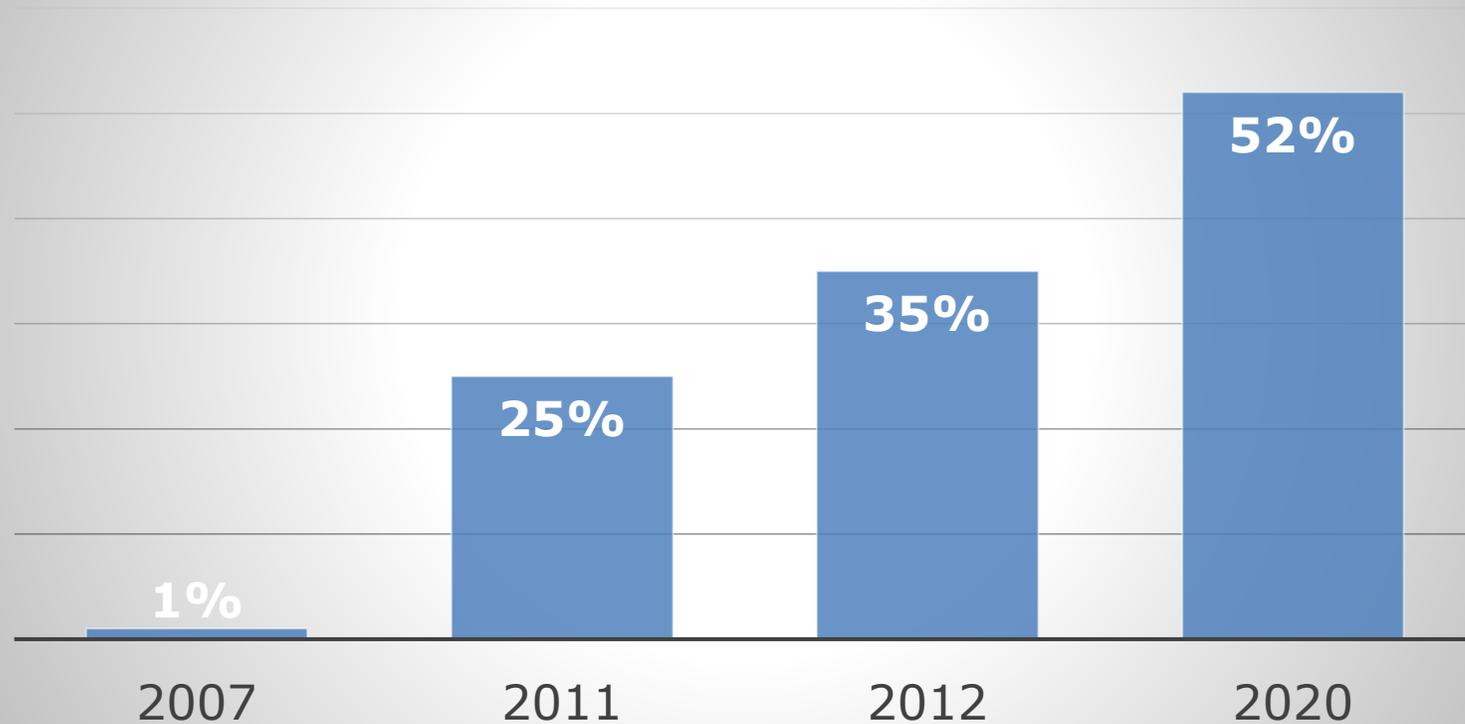


Mike Molitor

- Pilot Plant Manager for the Center for Dairy Research
- Filtration expert



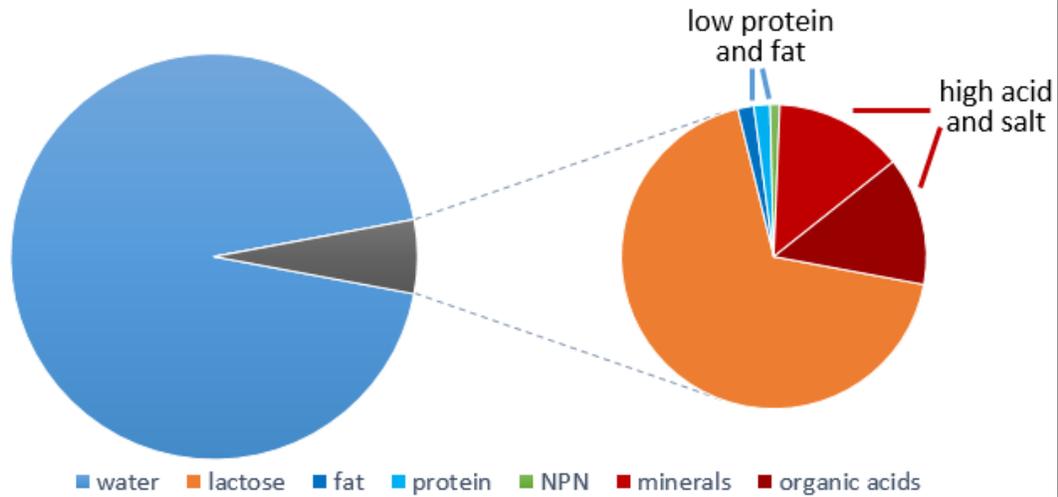
Market Share of Greek Yogurt in US



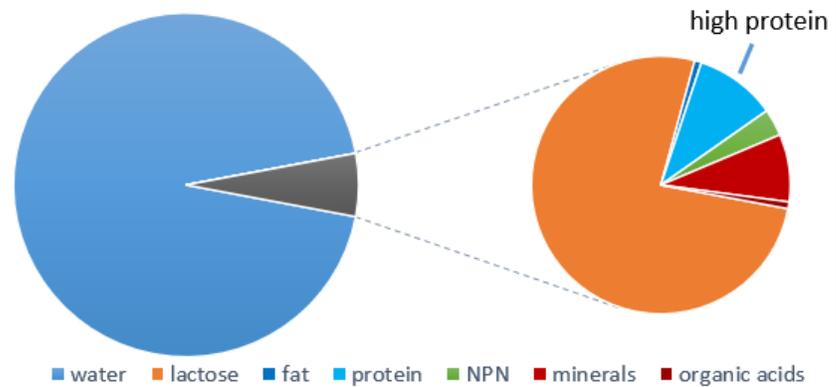
- 2-3 lbs Greek yogurt acid whey (GAW) per pound Greek yogurt
- 2 million tons GAW/year



Composition of GAW (wt%)



Composition of cheese whey (wt%)



Greek yogurt acid w





Whey protein



Whey powder



Lactose





- Land spreading
- Animal feed
- Wastewater treatment facility



- Environmentally unsustainable
- Expensive



Why are cheese whey treatment methods not used for GAW?

- Low Protein
- Sticky
- Hygroscopic lactic acid



End Results of Drying Problem Whey



Increased rate of
Maillard browning



Blocked valve



Scorch



Clumping



Material sticking to dryer
walls



Problem: Current GAW treatment methods are economically and environmentally unsustainable



Problem: Current GAW treatment methods are economically and environmentally unsustainable

Goal: Produce economically-viable high-value products from GAW

Product 1 – Glucose-galactose syrup (GGS)

- **Catalytic** lactose hydrolysis
- Test in **Ice Cream**

Product 2 – milk minerals

- **Filtration**

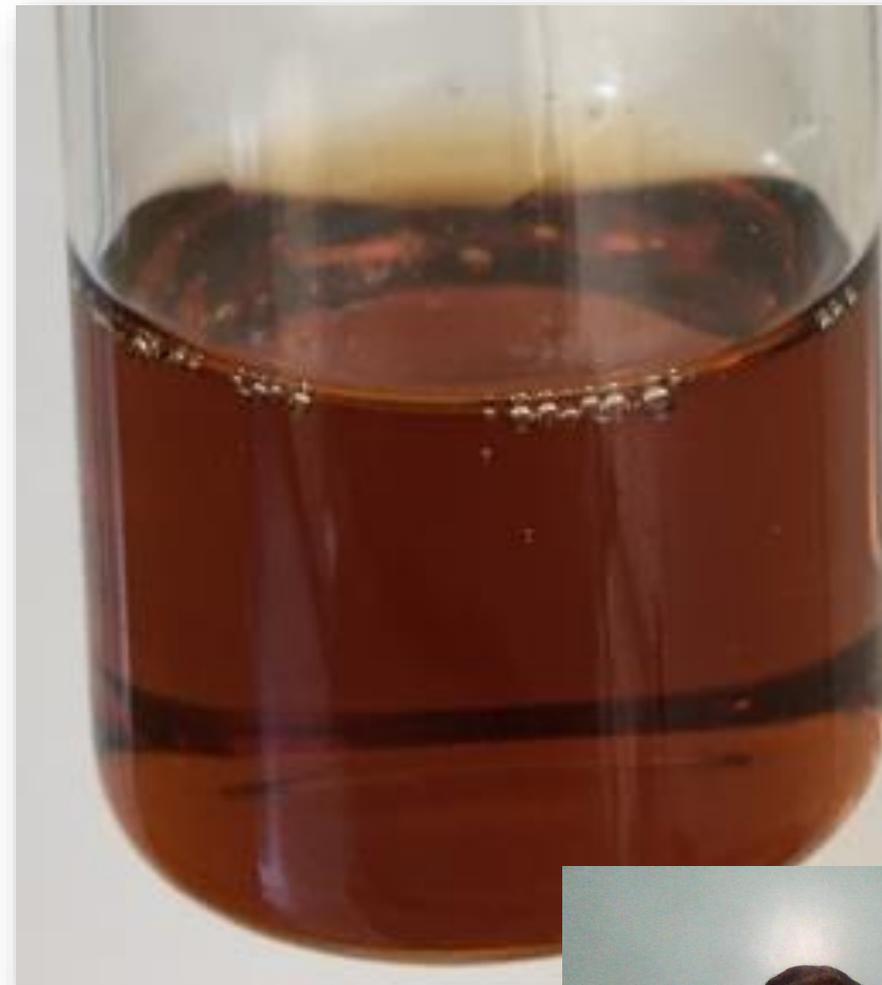


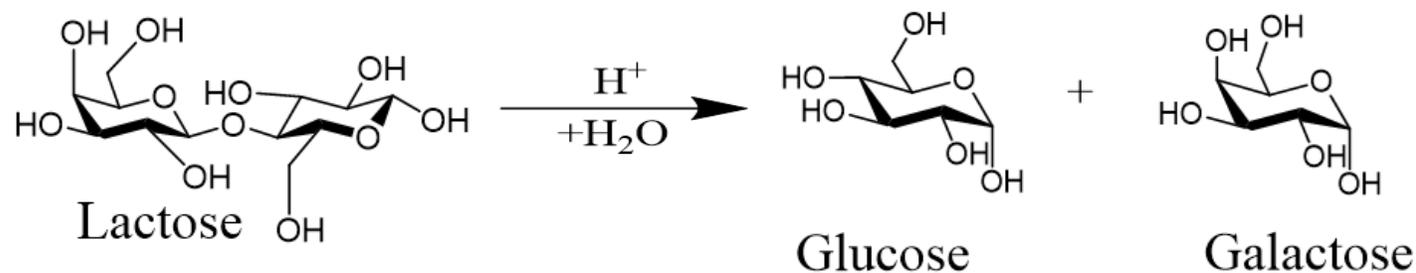
Glucose-galactose syrup



Glucose-galactose Syrup (GGS)

- **Uses:** Sweetener
 - Could replace high fructose corn syrup (HFCS)
- **Price:** N/A
 - HFCS-42 is \$510/ton
- **Note:** marketing advantages



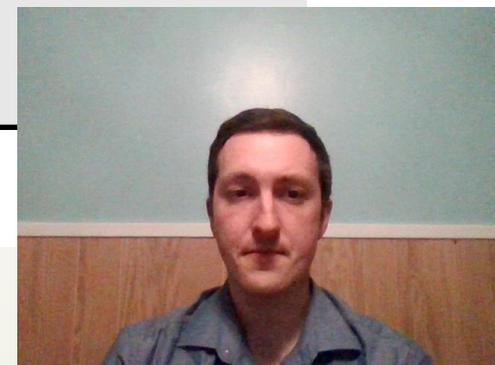


Acid-catalyzed lactose hydrolysis

- Increases sweetness
- More economical than enzymatic^{1,2}

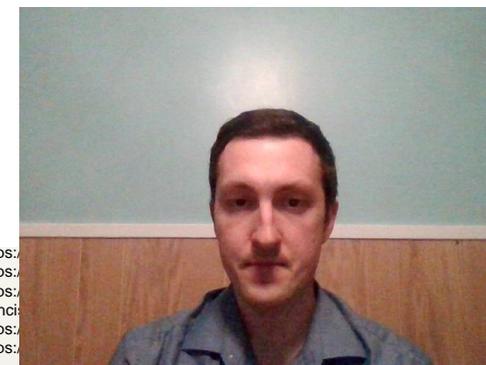
Sugar	Relative Sweetness
Sucrose (table sugar)	100
Lactose	16
Glucose	74
Galactose	60
High Fructose Corn Syrup 42	

1. R. de Boer and T. Robbertsen, *Neth. Milk Dairy J.*, 1981, 35, 95–111.
 2. M. R. Okos, E. A. Grulke & A. Syverson, *J. Fd Sci.* **43** (1978) 566-571.



Food made with GGS replacing some sugar	Result
Ice cream	Reduced off-flavors ² , smoother ³ , softer ³ , better overall ²
Soft-serve	Reduced off-flavors, better overall ⁴
Bread/bakery	Better overall ^{1,5}

•Note: marketing advantages (“green”, “no corn syrup,” “reduced waste”, “no added sugar”)



- Industrial filtration operations
 - Nanofiltration, ultrafiltration, microfiltration, and reverse osmosis
 - Allows separation of brine and livestock feed
- Spray dryer
 - Produces powder products
 - We produced milk minerals from filtered GAW in the spray dryer



Filter unit



Filtration system



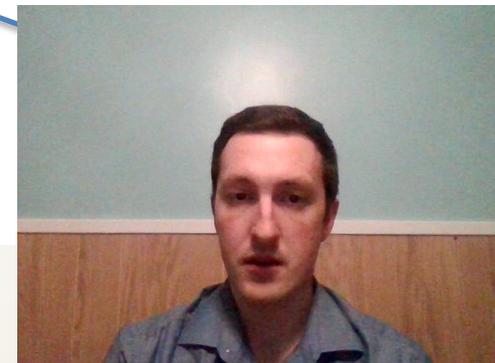
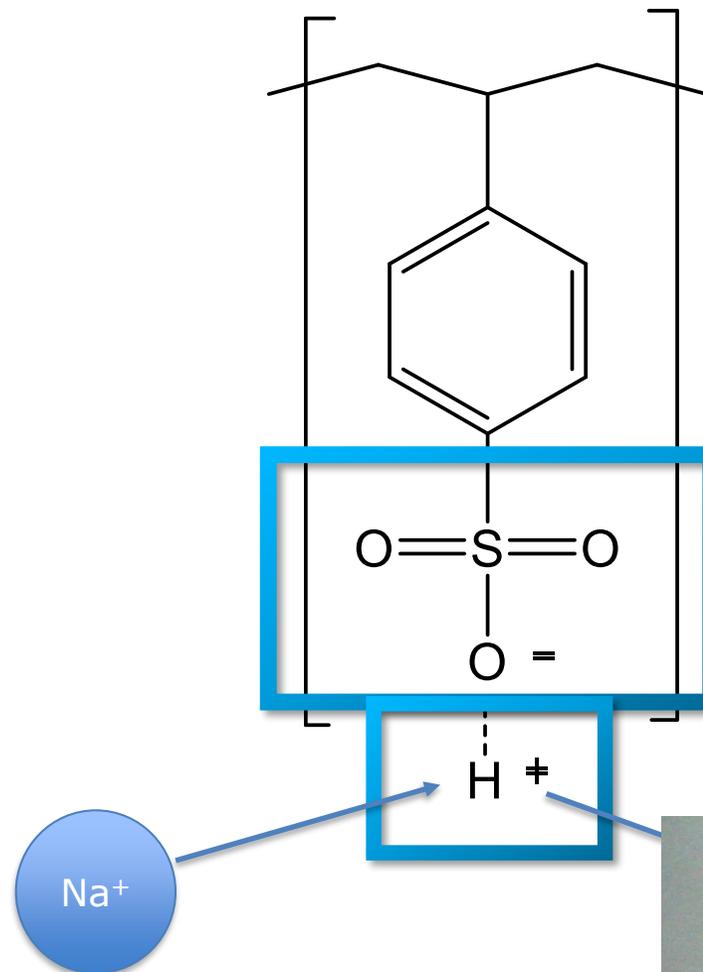
MF retentate



Spray dryer

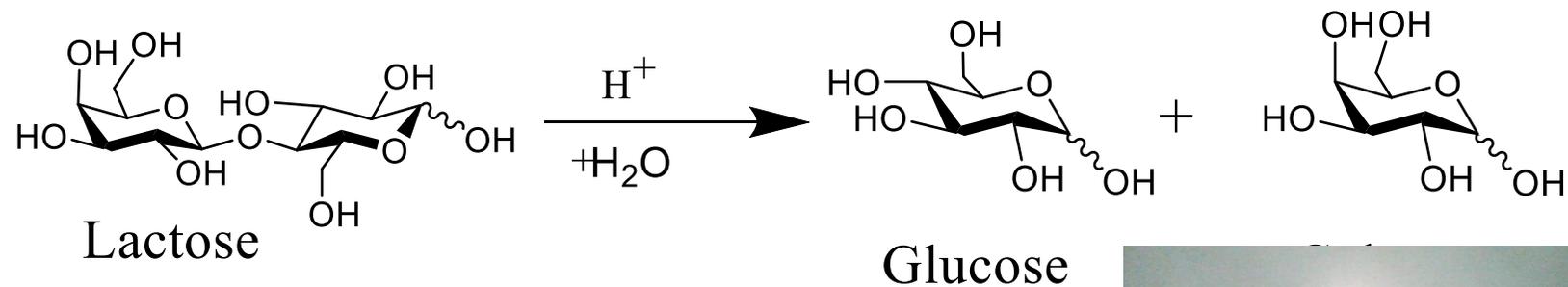


- Laboratory-scale ion exchange resins used
- Ion exchange resins adsorb:
 - Ions
 - NPN
 - Other impurities

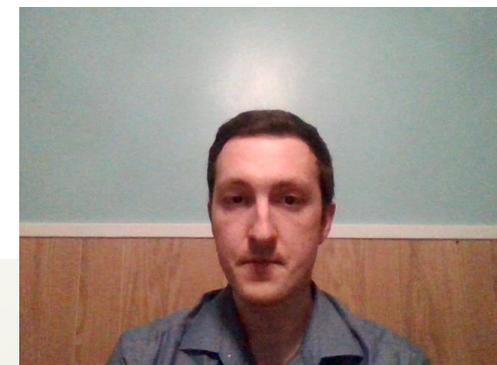
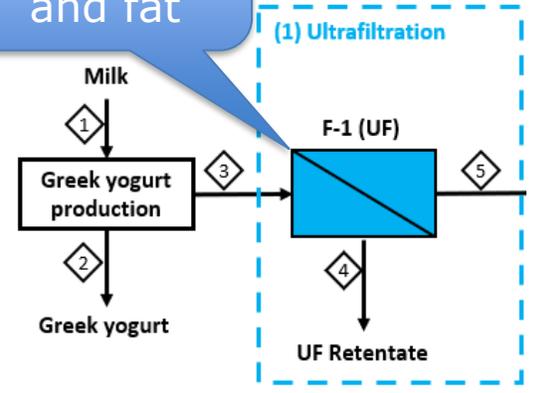


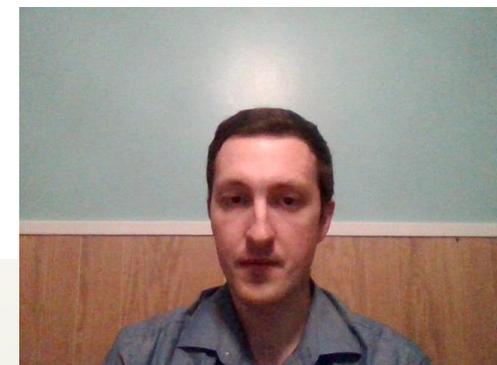
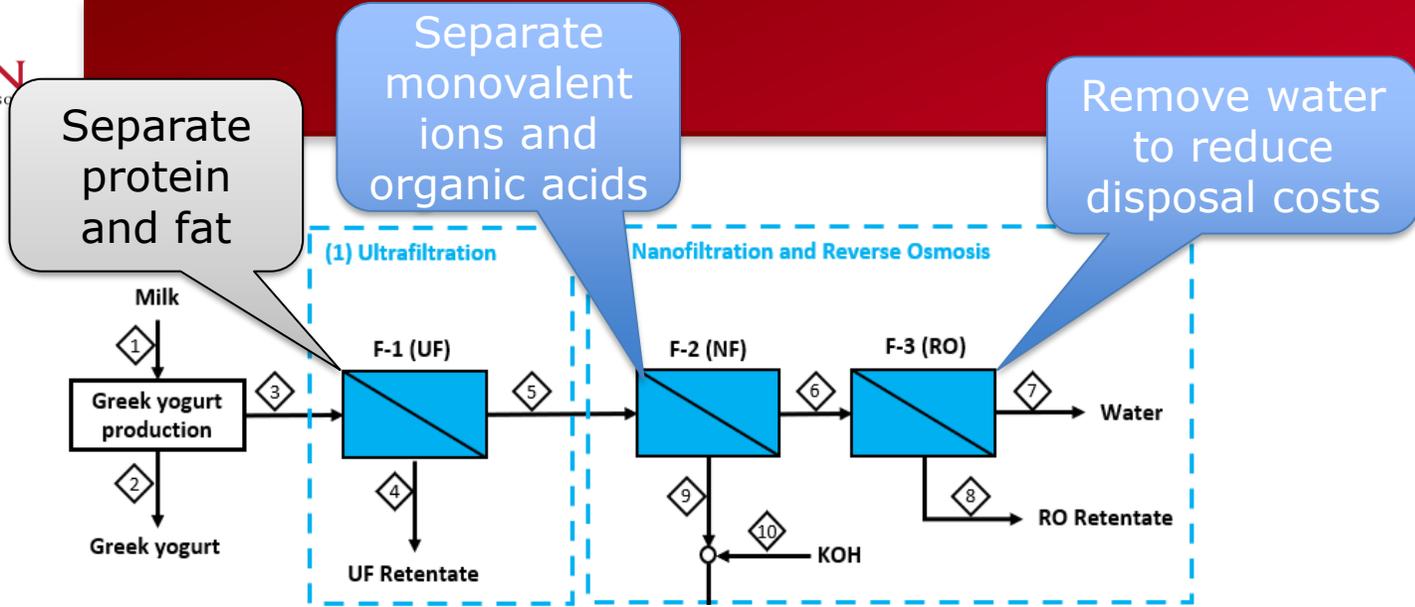


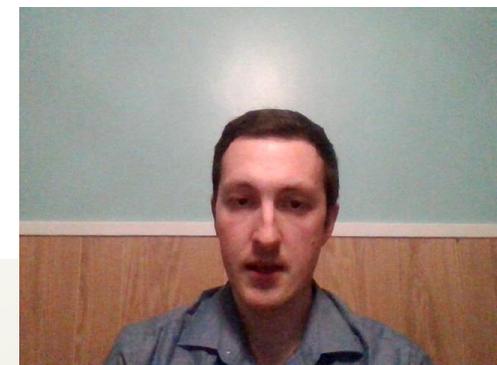
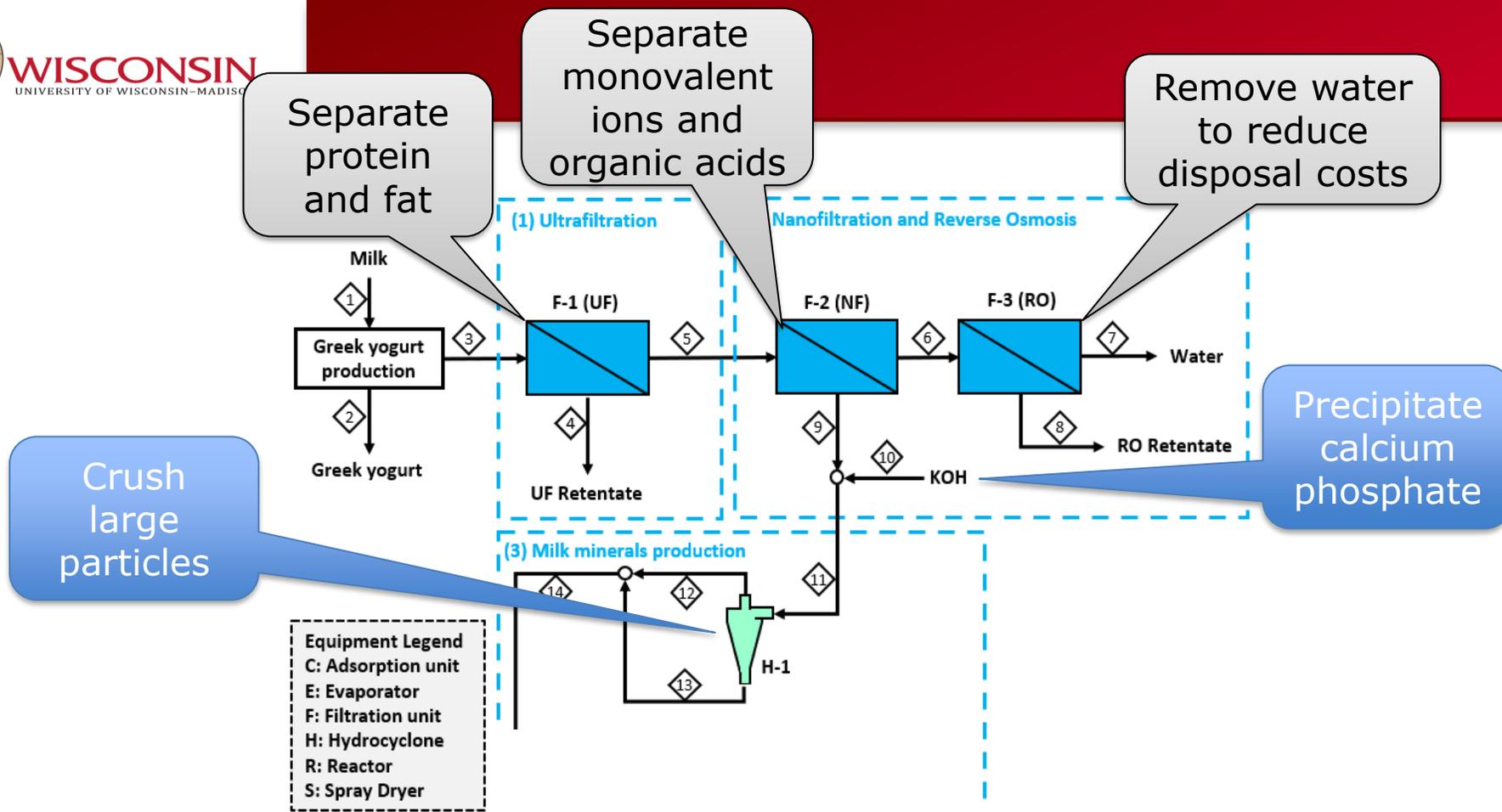
Lactose conversion	Glucose and Galactose Selectivity	Glucose and Galactose Yield
90%	99%	90%

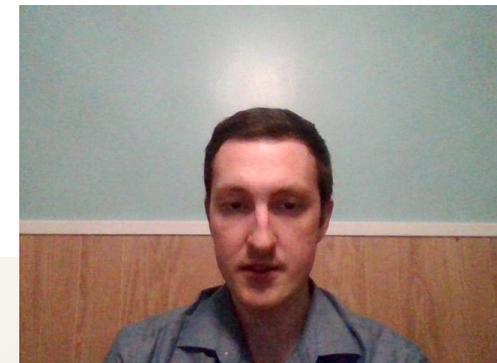
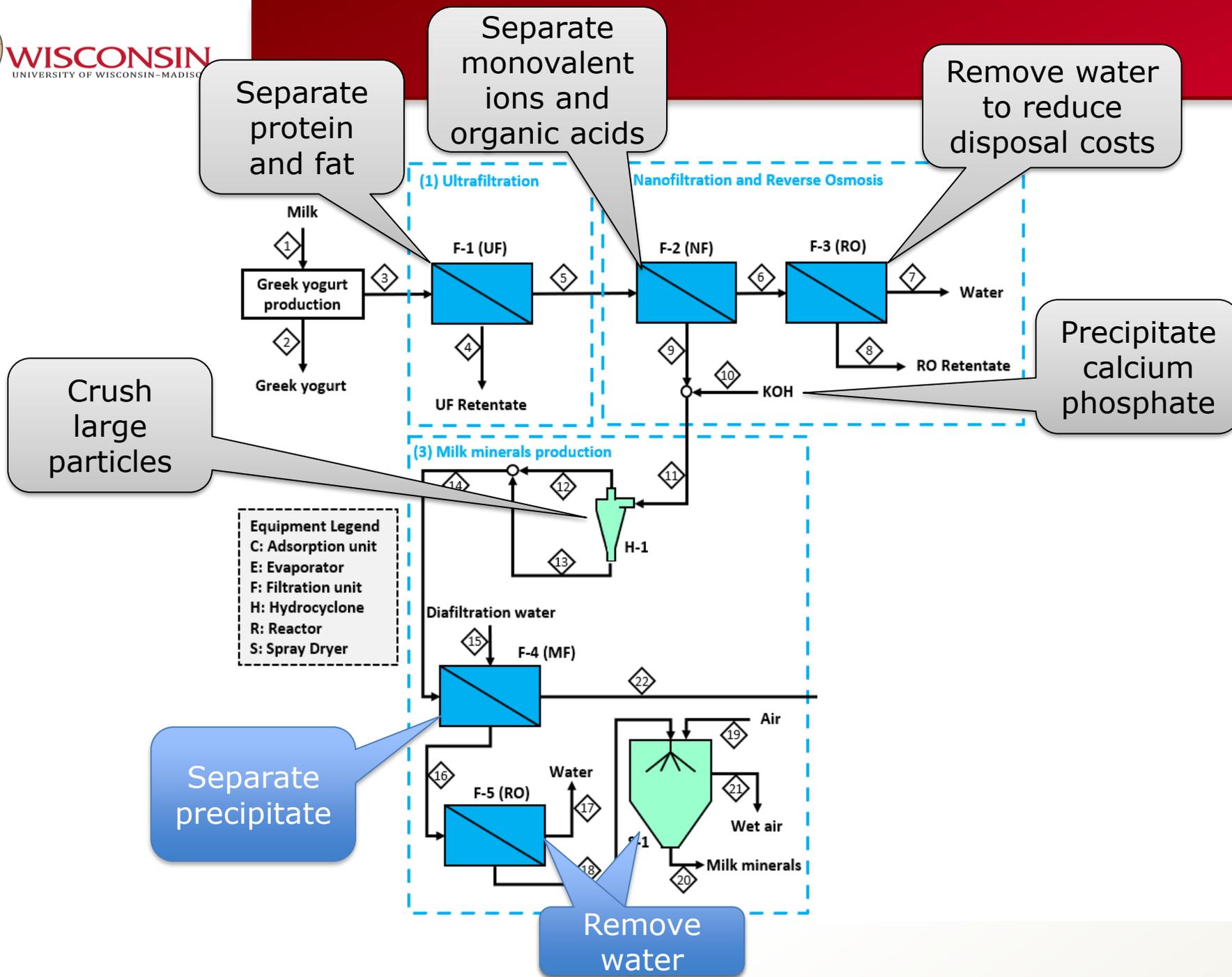


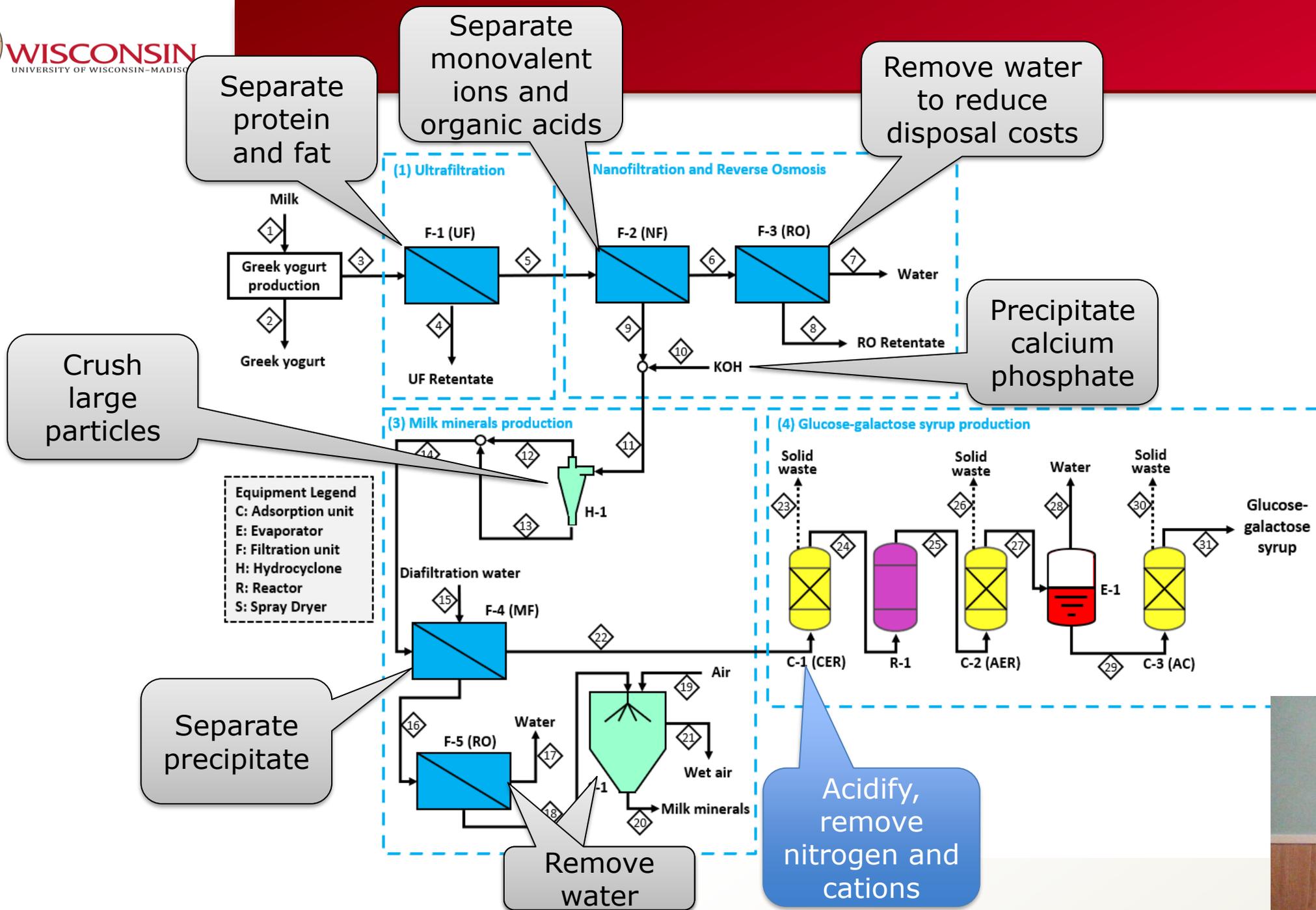
Separate protein and fat

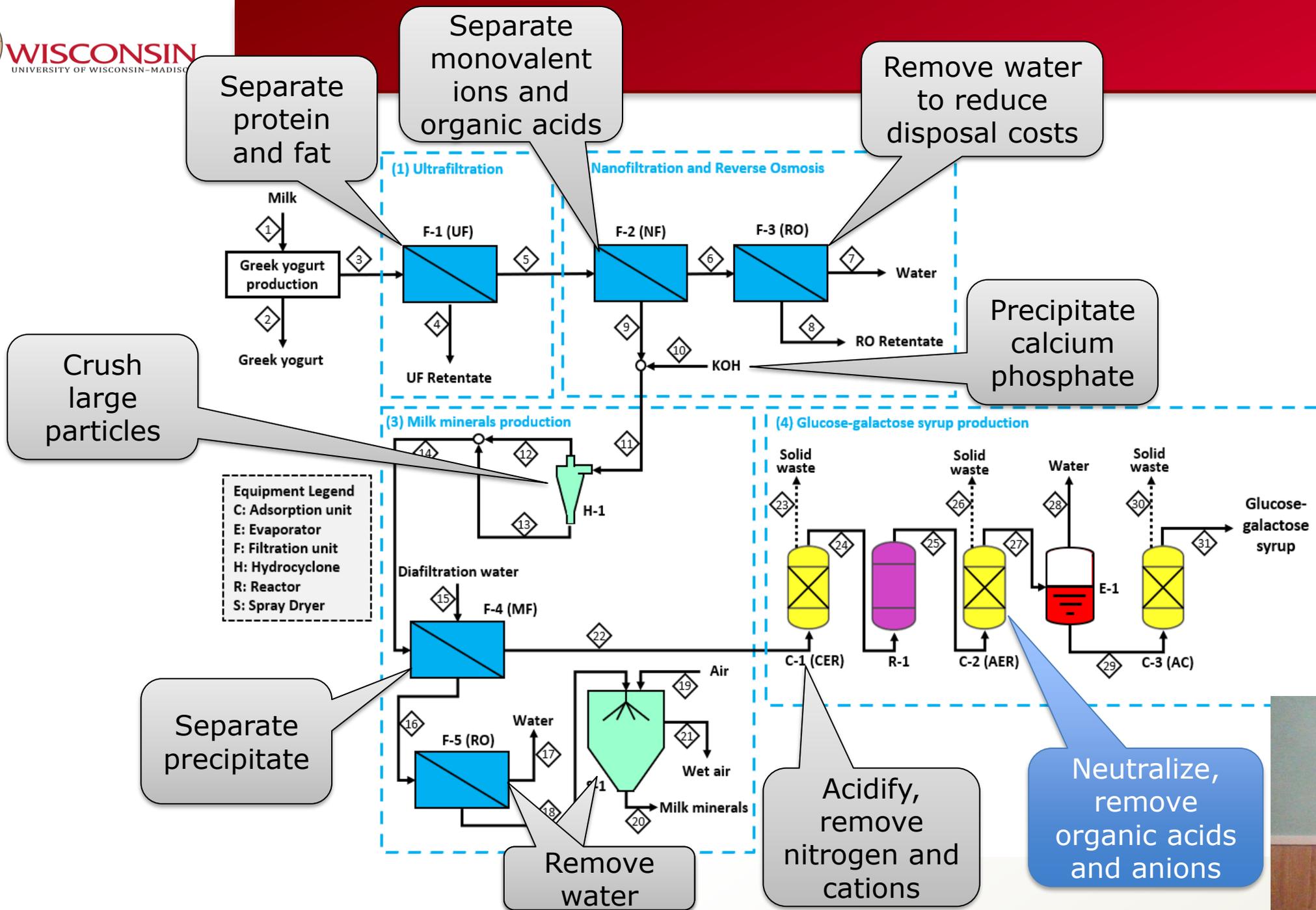


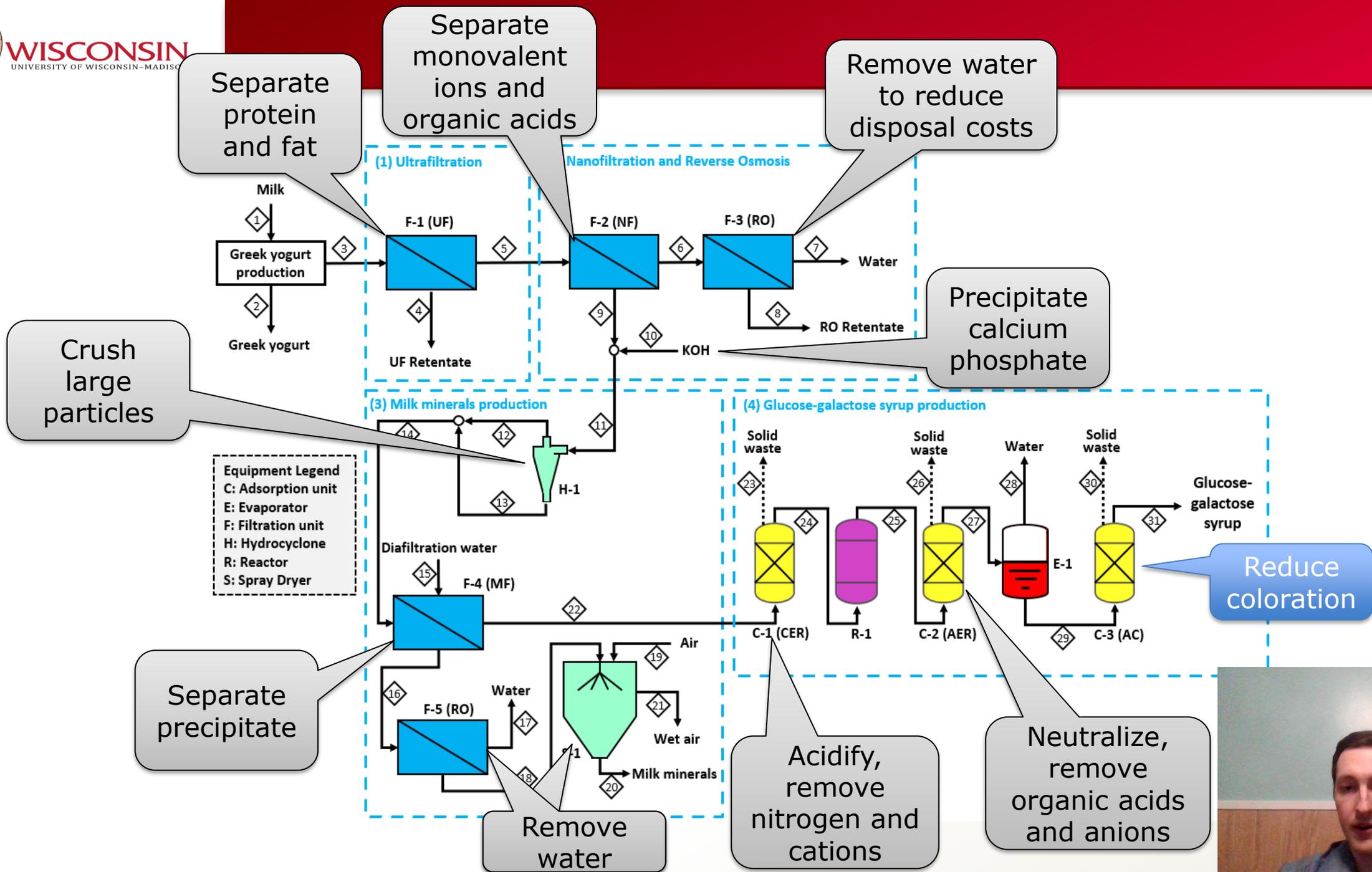


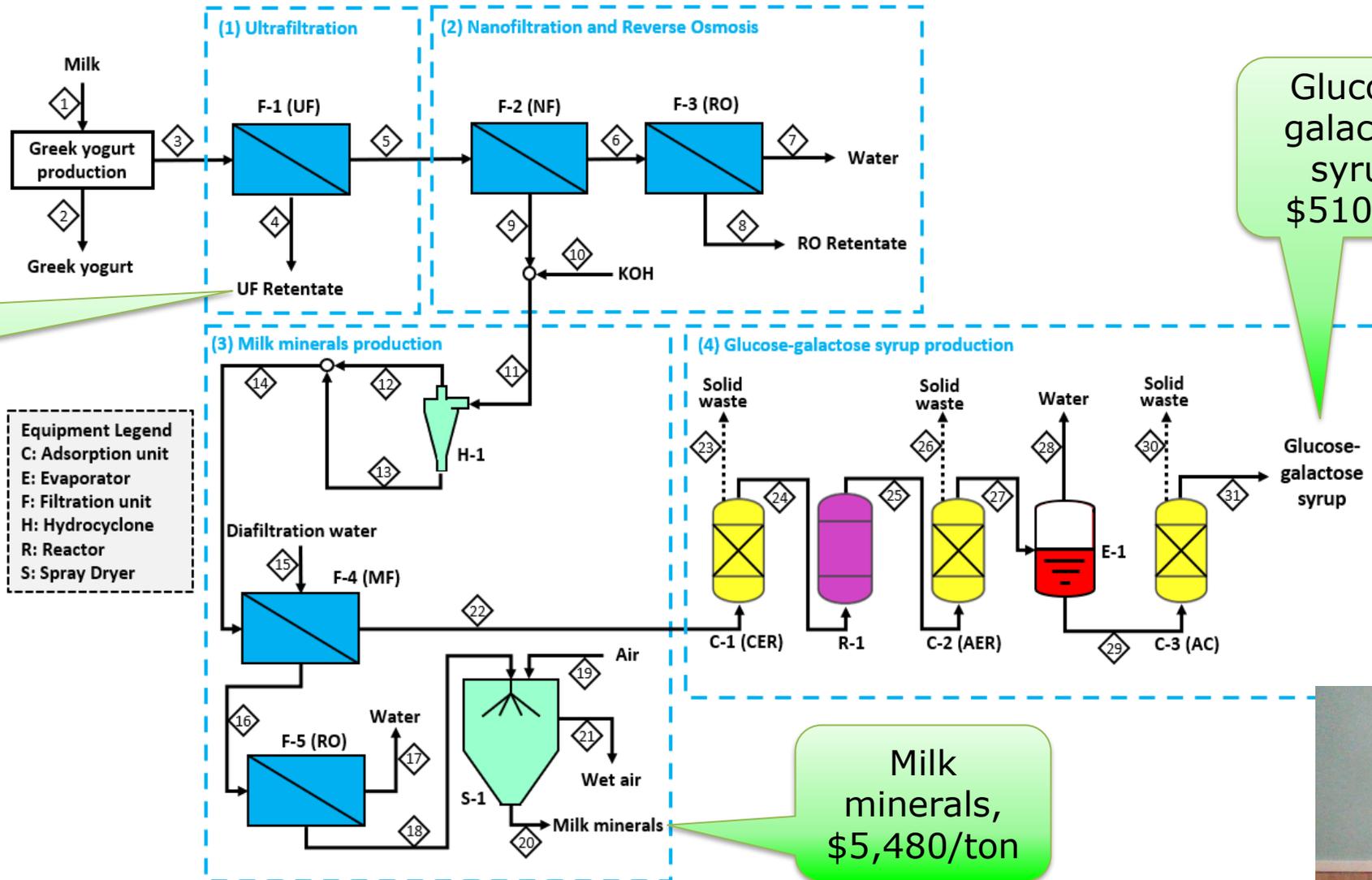








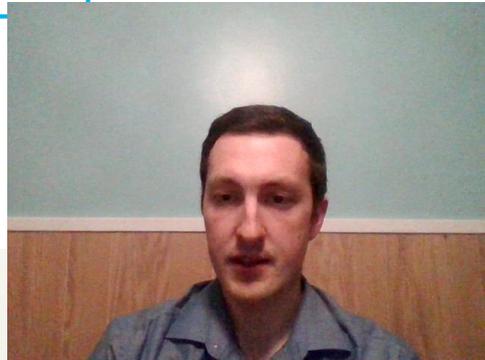




Sell as animal feed, \$110/ton

Glucose-galactose syrup, \$510/ton

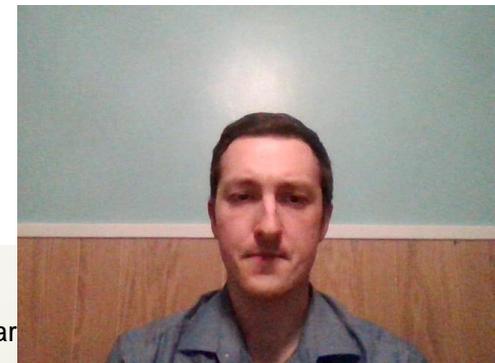
Milk minerals, \$5,480/ton



- Made 800 mL of GGS
- Fixed fish and sulfur flavors
- Now GGS tastes great!
 - Like maple syrup

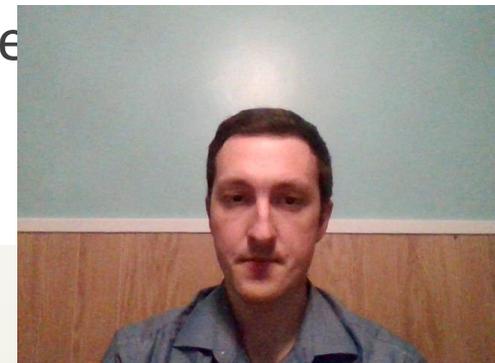


- 3 soft serve ice cream batches
 - Control (no GGS)
 - Test 1 (25% of sucrose replaced with GGS)
 - Test 2 (50% of sucrose replaced with GGS)
- Normalized to same freezing point
- Evaluated by 2 person expert panel

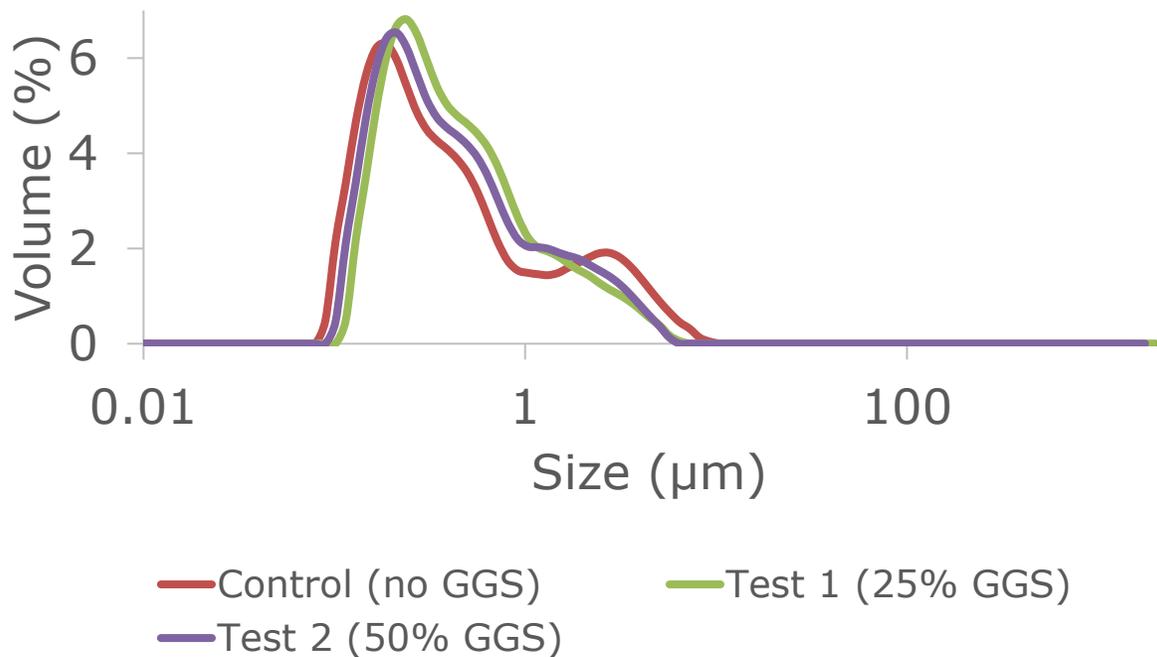


	Flavor	Cooked	Unnatural Flavor	Icy	Weak
Control	2	1	0	4	3
25% GGS	3	2	2	3	2
50% GGS	4	2	3	4	2

- Unnatural flavor was slight caramel
- 0s for 18 descriptors, including:
 - acid, syrup flavor, greasy, gummy, low flavoring, low sweet

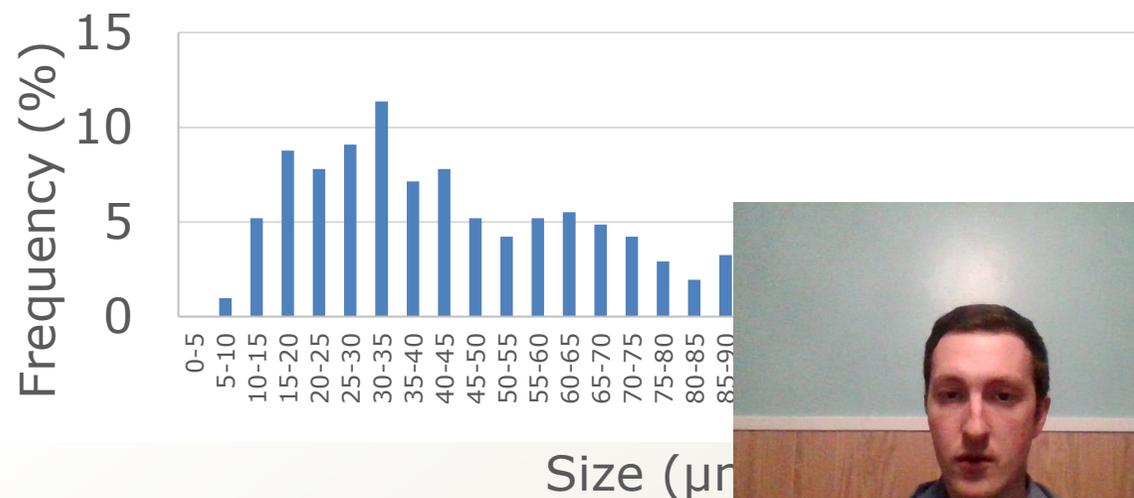


Ice Cream Fat Globule Size

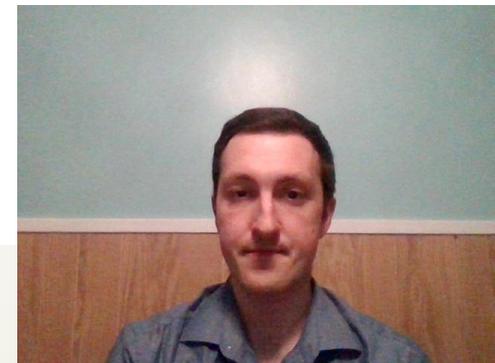


Soft Serve Batch	Mean Size (μm)	Std. Dev (μm)
Control (no GGS)	45.1	24.3
Test 1 (25% GGS)	51.0	22.2
Test 2 (50% GGS)	43.3	21.0

Ice Crystal Size

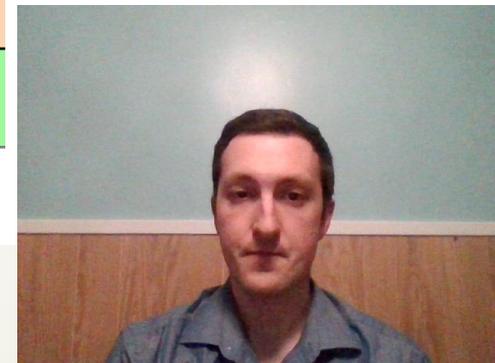


Assumption	Value
GAW Feed price (\$/ton)	0
GAW Feed (tons/day)	1,000
GAW disposal cost (\$/ton)	16 ¹
Contingency (%)	40
Plant life (years)	30



Product	Value (\$/ton)	Flow (tons/day)	Value (\$ million/year)
GAW disposal credit	16	1,000.0	5.3
GGs (wet basis)	510	54.6	9.2
Milk minerals	5,480	1.6	3.0
UF retentate (sold as animal feed)	110	52.1	1.9
Total Revenue			19.3

Capital costs	33.5	\$ million
Operating costs	5.8	\$ million/yr
Income tax	2.7	\$ million/yr
After tax net revenue	10.2	\$ million/yr



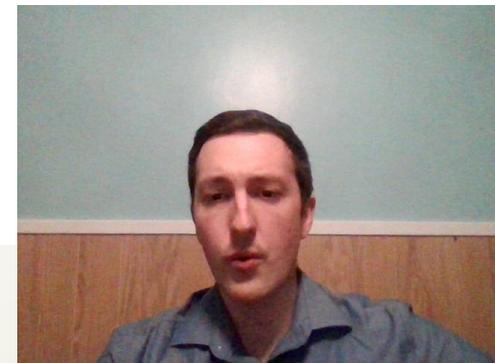
- Discounted Cash Flow Rate of Return analysis (DCFROR)
 - Accounts for present vs future value of money

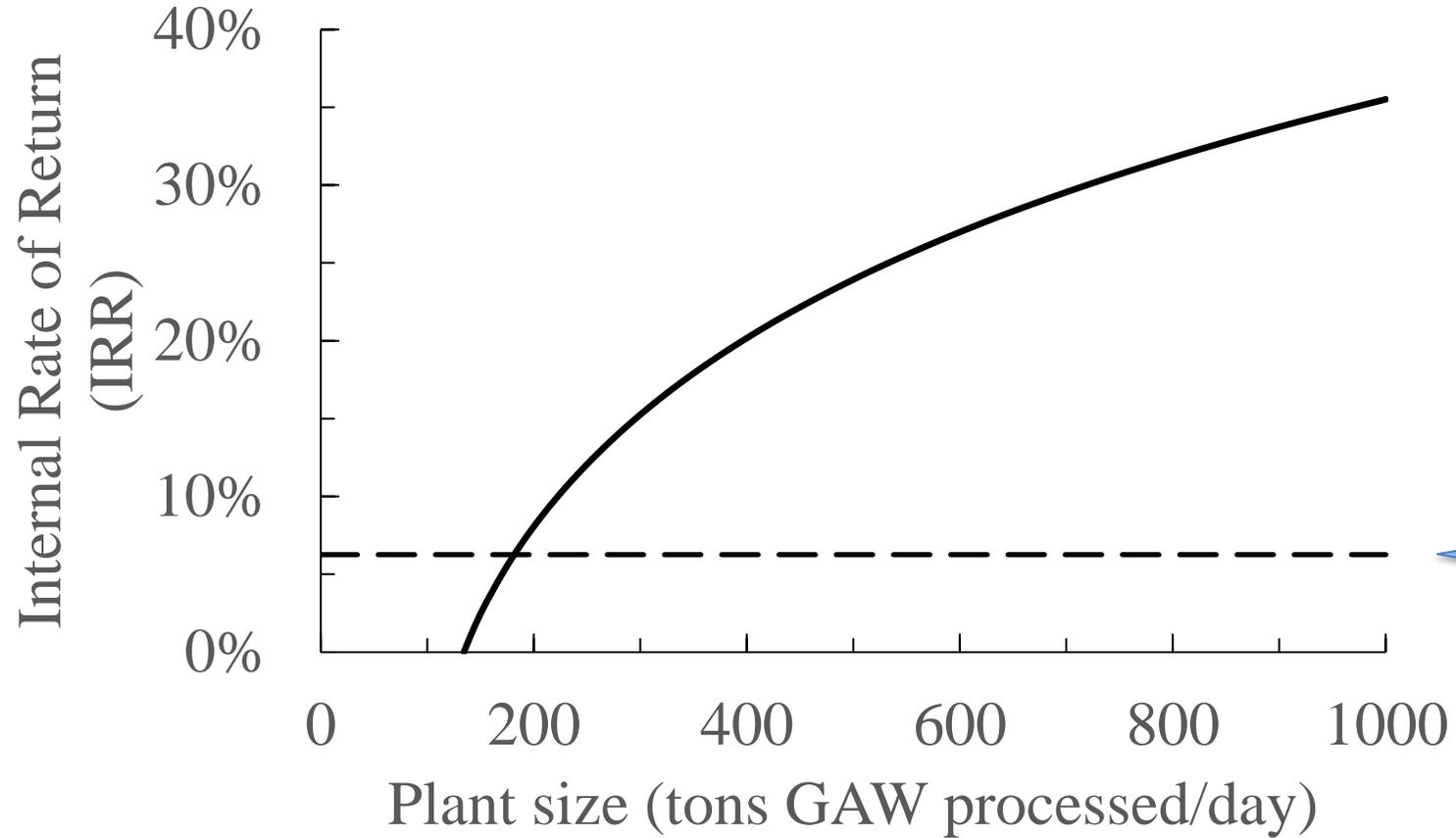
Capital costs (\$ million)	33.5
After tax net revenue (\$ million/yr)	10.2
IRR (%)	35.5



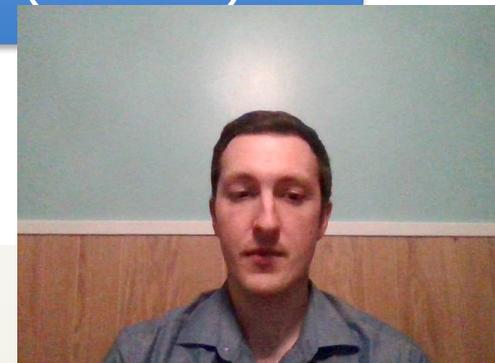
- Discounted Cash Flow Rate of Return analysis (DCFROR)
 - Accounts for present vs future value of money

Capital costs (\$ million)	33.5
After tax net revenue (\$ million/yr)	10.2
IRR (%)	35.5
IRR without GAW disposal credit (%)	21.7





Food industry
average¹
(6.25%)



- Scale up to pilot-scale
 - Jarryd Featherman heads this
 - Goal: produce >1 gal/month of GGS
- Use this technology in other low-value dairy streams
 - can be adapted to any stream with lactose
 - de-lactosed permeate, other acid whey, etc.
- Find industrial collaborators interested in using or commercializing the technology

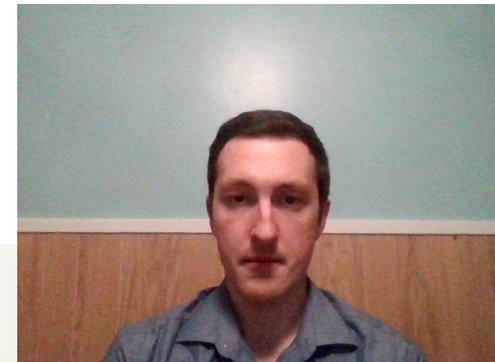


- Patent application filed
 - Huber, George W., Scott A. Rankin, and Mark J. Lindsay. "Method of converting lactose-containing dairy by-products into monosaccharides." U.S. Patent Application No. 15/926,461.
- 2 publications
 - Lindsay, Mark J., et al. "Production of monosaccharides and whey protein from acid whey waste streams in the dairy industry." *Green Chemistry* 20.8 (2018): 1824-1834.
 - Lindsay, Mark J., et al. "Catalytic Production of Glucose-Galactose Syrup from Greek Yogurt Acid Whey in a Continuous Flow Reactor." *ChemSusChem*

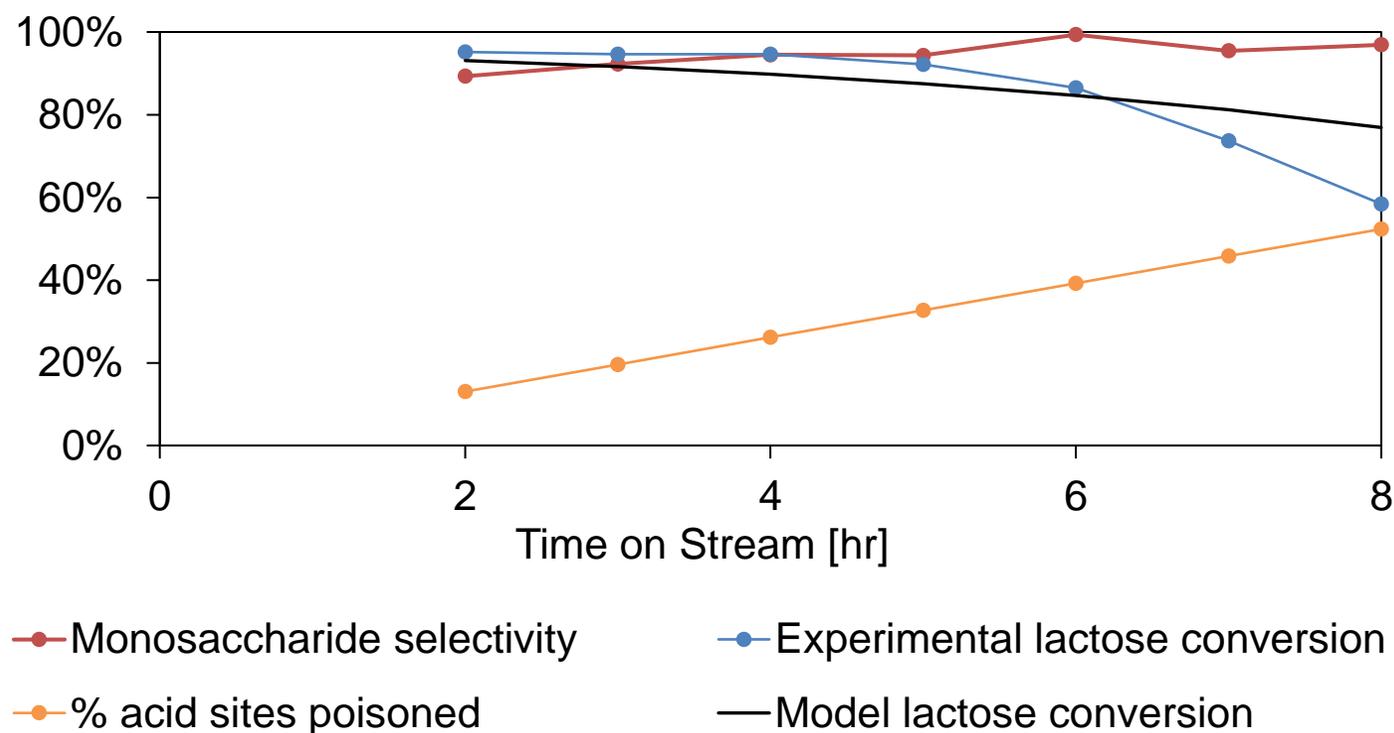




Questions?



- 1 demineralization step
- 4 hours at >80% lactose conversion



Row	Process Area	Calculation method	Installed Cost (\$ million)
1	1. UF		2.0
2	2. NF and RO		2.8
3	3. Milk minerals production		2.8
4	4. GGS production		6.1
5	ISBL	=1+2+3+4	13.6
6	Other OSBL (Storage ect.)		0.7
7	Warehouse	4.0% of ISBL	0.5
8	Site Development	9.0% of ISBL	1.2
9	Additional Piping	4.5% of ISBL	0.6
10	Total Direct Costs (TDC)	=5+6+7+8+9	16.7
11	Prorateable Expenses	10.0% of TDC	1.7
12	Field Expenses	10.0% of TDC	1.7
13	Home Office & Construction Fee	20.0% of TDC	3.3
14	Project Contingency	40.0% of TDC	6.7
15	Other Costs (Start-Up, Permits, etc.)	10.0% of TDC	1.7
16	Total Indirect Costs	=11+12+13+14+15	15.0
17	Fixed Capital Investment (FCI)	=10+16	31.8
18	Land & Working Capital	5.5% of FCI	1.7
19	Total Capital Investment (TCI)	=17+18	33.5

- Aspen Plus process simulation software and industry quotes used for capital and utility costs

Raw Material	amount	unit	Price	Unit	\$ million/yr
Sulfuric acid (98% food grade)	13	tons/day	200	\$/ton	0.83
sodium hydroxide	5	tons/day	350	\$/ton	0.59
Ion exchange resins					0.02
Filter replacements and CIP					2.07
RO retentate disposal	100	tons/day	16	\$/ton	0.53
Process water	440	tons/day	0.29	\$/ton	0.00
Low Pressure Steam	4,859	kw	1.90E-6	\$/kJ	0.26
Cooling Water	264	kw	2.12E-7	\$/kJ	0.00
Grid Electricity	16	kw	0.0691	\$/kWh	0.37
Total Variable Operating Costs					4.15

Position	Salary	# Required	Total	\$ million/yr
Plant engineer	\$ 91,283	1	\$ 91,283	
shift operators	\$ 47,333	10	\$ 454,397	
Total Salaries			\$ 545,680	0.55
Labor Burden (90%)			\$ 491,112	0.49
Maintenance	3.0% of ISBL		\$ 409,525	0.41
Property Insur. & Tax	0.7% of FCI		\$ 222,406	0.22
Total Fixed Operating Costs				1.67
Total Operating Costs				5.81